

The Use of Hydrotropic Solutions for Counter-Current Separations

Journal Article

Author(s): Winistorfer, Peggy; Kováts, E. Sz.

Publication date: 1967

Permanent link: https://doi.org/10.3929/ethz-b-000422791

Rights / license: In Copyright - Non-Commercial Use Permitted

Originally published in: Journal of Chromatographic Science 5(7), <u>https://doi.org/10.1093/chromsci/5.7.362</u>

This page was generated automatically upon download from the <u>ETH Zurich Research Collection</u>. For more information, please consult the <u>Terms of use</u>.

The Use of Hydrotropic Solutions for Counter-Current Separations

by **Peggy Winistorfer** and **E. sz. Kováts,** Swiss Federal Institute of Technology, Department of Industrial and Engineering Chemistry, Zurich, Switzerland

The selective dissolving properties of aqueous solutions of hydrotropically active salts* suggest their application as one of the phases in counter-current distribution. However, since hydrotropic activity parallels surface activity (1), such solutions emulsify on shaking with a second solvent; therefore, their use in classical counter-current distribution has been severely limited. Recently, a new variant of an apparatus was realised (2 and 3) following the original proposal of Signer et al. (4) in which shaking the phases is avoided. Such an apparatus has not yet been described in full detail⁺. In the present paper, the principle of this method will be explained together with an apparatus of our own construction.

A glass tube is separated into cells (see Figure 1) by the insertion of Teflon disks pierced by a small hole through the center. The more dense solvent which serves as the stationary phase is filled into the cells, its final level being lower than the central hole. The less dense solvent is pumped continuously into the first cell, filling it up to the central hole (the direction of flow is indicated by an arrow in Figure 1), and then passes through the hole to the second cell, to the third cell, etc. Equilibration of the two phases is effected within each cell by rotating the glass tube about its central axis. This rotational movement mixes the two phases and continuously renews their contact surface, leading to equilibration times comparable to those obtained by shaking but without causing foaming. The upper phase is prevented from flowing from one cell to the next without effective mixing by the insertion of smoothly curved stainless steel plates; these also add to the efficiency of the equilibration by longitudinal mixing. Figure 2 shows the whole assembly, the operation of which is described in detail in the experimental part. Essentially, the eluent is pumped through a series of rotating tubes which are parted into cells (in this case, 8 tubes containing 650 cells).

For the application of solutions of hydrotropically active salts in counter-current distribution, a thorough knowledge of their dissolving properties against different classes of substances would be desirable. In the first treatment of hydrotropy, Neuberg (6) investigated the hydrotropic activity of several different salts on a variety of substances by looking at the saturation concentrations. This work only gives information about the solubility of pure substances, thus taking the pure substance as standard state. More recently, Rath, Rau, and Wagner (1 and 7) investigated the dissolving power of many salts but on only one substance.

We have chosen as standard state the ideal diluted solution in a pure one-component non-polar system [non-polarity is defined as a nonpolar substance being only a pure paraffin or mixture of paraffins, C_nH_{2n+2} (8 and 9)]. By equilibrating solutions of given substances in n-heptane with solutions of hydrotropically active salts, the partition coefficient clearly defines the chemical potential of the substance in the salt-solution with respect to the standard state in n-heptane. In

*In the literature the terms "hydrotropes" and "hydrotropic substances" are used. The definition of a "hydrotrope" should then be: "a substance which changes the solvent properties of water," implying obviously all water soluble substances. We propose to drop these terms and to speak of the "hydrotropic activity" of a substance and of "hydrotropy" for the effect.

+Private communication from Prof. Dr. R. Signer: The apparatus used for separations in ref. (2) and (3) will be described in a forthcoming paper (5). this way one can even examine substances which are completely miscible with both solvents.

It has been suggested that hydrotropic action arises mainly through interactions of polar parts of the solute with the organic ion of the salt (1 and 7). For this reason two neutral salts were selected, one having a negatively-charged organic ion — potassium-1-octylsulfonate, and the other having a positivelycharged ion — trimethyl-1-octylammoniumbromide. The organic part of each salt contains the same, non-polar octyl residue.

Figure 3 shows the logarithms of the partition coefficients K_c plotted against the percentage concentration (in g/100 ml) of the two salts, where K_c is defined in equation 1.

Eq. 1

The same results are shown in Figure 4 but are expressed as K_x against molality, where K_x is defined in equation 2

 $K_x =$

mole fraction of the substance in heptane mole fraction of the substance in the salt sol. Eq. 2

Neither presentation suggests a



Figure 1. Sectional view of glass counter-current distribution tube showing individual cells.

simple interpretation. At low salt concentrations the partition coefficients are more or less constant. For potassium-1-octylsulfonate at about 3% concentration and for trimethyl-1-octylammoniumbromide at 4% concentration, there is an apparent discontinuity in the shape of the curves. A hydrotropic action of the salts begins actually only at higher concentrations. A possible explanation is that initially the very ordered structure of water is broken down.

In the two figures (3 and 4) the numbered curves belong to the homologuous series of primary alcohols (2:ethanol, 3:propanol, etc., up to 12:dodecanol). The alcohols have lower partition coefficients in



Figure 2. Counter-current distribution apparatus showing rotating tube assembly and feed system.



the solutions of potassium-1-octylsulfonate compared with those of trimethyl-1-octylammoniumbromide. This supports the suggestion of Rath, et al. (7) that in the case of alcohols, one of the main solubilising effects is through hydrogenbonding to the negatively-charged organic ion (in our case, of the 1octylsulfonate ion).

Figure 5 shows the logarithms of K_x plotted against the carbon-numbers of the alcohols. This plot is linear for the distribution between heptane and pure water. However, in the case of the distribution between heptane and salt solutions, the lines are curved for the lower alcohols tending to linearity for the higher members, with decreasing slope for increasing concentration of the salt.

To detect further differences between the action of the two salts, four additional compounds of distinctly different types were investigated. These are indicated by capital letters in Figures 3 and 4 (A: 1-octylacetate, C: 1-chlorooctane, E: dipentylether, K: nonanone-(2)). The results for these compounds are difficult to rationalise in any simple scheme. For example, the ketone (K) has a relatively low partition coefficient in both salt solutions. The ether (E) has a preferential solubility in the cationic solvent. Thus, simple arguments might suggest that the acetate (A) which contains both ether and ketone functions should preferentially dissolve in the solutions of trimethyl-1-octylammoniumbromide. However, the contrary is the case.

The results of the present investigation show that the mechanism of hydrotropic action requires much more thorough examination. However, they also show that such solutions are capable of being used as stationary phases for counter-current distribution. The order of the elution would be non-polar substances and substances of low polarity (hydrocarbons), followed by more polar compounds (ethers, esters, aldehydes, ketones, etc.), and finally alcohols. In a homologous series the higher members are eluted first. Preliminary attempts to achieve separations using a solution of potassium-1-octvlsulfonate as stationary phase in our countercurrent apparatus are promising.

Experimental

Materials

Potassium-1-octylsulfonate was synthesised by the method of Backer (10). Octyl bromide (257 g, 1.33 mole) was heated with an aqueous solution of sodium sulfite (193 g sodium sulfite, 1.54 mole in 750 ml water) in a copper autoclave at 170° C for 14 hrs. To the resulting hot reaction mixture, sodium chloride (200 g) was added. By cooling the solution the sulfonate could be obtained as a wet crust. The product was freed from water by pressing in a cloth, and the air-dried product was crystallised from absolute ethanol.

An aqueous solution of the sodium sulfonate was filtered onto



an ion exchange column (2000 g Dowex 50 W, 20-50 mesh, prepared as potassium salt). The resulting solution of the potassium sulfonate was evaporated to dryness and the solid product recrystallised from ethanol giving 227 g (75%) potassium-1-octylsulfonate as white crystals.

	С	\mathbf{H}	K	
calc	41.35	7.38	16.83	%
found	41.26	7.18	16.85	%

Trimethyl-1-octylammoniumbromide: Octyl bromide (485 g, 2.51 mole) was mixed with trimethylamine (150 g, 2.54 mole) in a pressure flask and was allowed to stand for 72 hrs. at room temperature. The crude crystalline product was recrystallised from acetone giving 393 g (62%) trimethyl-1-octylammoniumbromide (m.p. $221/2^{\circ}C$).

	\mathbf{C}	\mathbf{H}	Ν	\mathbf{Br}	
calc.	52.38	10.39	5.55	31.68	%
found	52.24	10.45	5.70	31.51	%

Properties of the aqueous solutions of the two salts

Solubility of potassium-1-octylsulfonate: Saturated solutions of this salt were gelatinous and a quantitative value of the saturation concentration could not be obtained. The solubility of the salt was certainly over 47% at 0° and 22°C.

Solubility of trimethyl-1-octylammoniumbromide: Nearly saturated solutions of the salt in water were saturated by pressing through a thermostatted column filled with pills of the salt. Five ml. of the eluent was evaporated to dryness and weighed. Table I shows the saturation concentrations and the densities at different temperatures.

Table	١.	Saturation	concentra-
tions a	nd	densities of	trimethyl-1-
octylar	nm	oniumbromio	de in water.

temp.	g/100 g	density
<u>(</u> <u>0</u>)	<u> </u>	1.0867
5	68.7	1.0827
10	70.5	1.0827
15	70.7	1.0783
20	71.2	1.0746

Densities of aqueous solutions of the two salts: The densities of the solutions were determined in a pyknometer. Tables II and III show the experimental results.

Variance analysis of the results shown in Tables II and III resulted by proving the significance of $P_{c}, P_{cc}, P_{ccc}, P_{T}, P_{TT}, P_{c}P_{T}, P_{c}P_{TT}$ for potassium-1-octylsulfonate and $P_{\rm C}$, $P_{\rm T}$, $P_{\rm TT}$, $P_{\rm C}P_{\rm T}$ for trimethyl-1octylammoniumbromide at the 95% significance level ($P_{\rm C}$, $P_{\rm CC}$, $P_{\rm CCC}$ symbolizing the linear, quadratic, cubic, etc., orthogonal polynominals). Regression equations were calculated with the aid of the significant terms. They allow the calculation of the

Table II.	Densities of aqueous solutions of				
potassium-1-octylsulfonate					

concentration	temperature (°C)				
(g/g)	0	20	40	60	
0	0.9999	0.9982	0.9922	0.9832	
15	1.0426	1.0373	1.0281	1.0179	
30	1.0731	1.0652	1.0547	1.0432	
45	1.1121	1.1005	1.0888	1.0760	

Table III. Densities of aqueous solutions of trimethyl-1-octylammoniumbromide

concentration	temperature (°C)				
(g / g)	0	20	40	60	
0	0.9999	0.9982	0.9922	0.9827	
16.7	1.0199	1.0147	1.0070	0.9965	
33.3	1.0405	1.0327	1.0227	1.0102	
50.0	1.0606	1.0492	1.0404	1.0266	

Table IV. Concentrations of the aqueous solutions used of potassium-1-octylsulfonate at 20°C

\mathbf{g}/\mathbf{g}	g/cm³	cm ³ /cm ³	gmol gmol	gmol $g(H_2O)$	${ m cm^3} { m cm^3} ({ m H_2}{ m O}$	gmol)	g/cm³
c' 100	с 100	а 100	x 100	m 1000	β 1000	Μ	d ₂₀
0.0000	0.0000	0.0000	0.0000	, 0.00000	0.000	18.016	0.9982
0.0953	0.0952	0.0635	0.0073	0.00410	0.635	18.031	0.9989
0.4322	0.4322	0.292	0.0336	0.01867	2.928	18.088	1.0001
1.1201	1.1227	0.768	0.0877	0.04874	7.739	18.204	1.0023
2.317	2.330	1.627	0.1835	0.10206	16.539	18.409	1.0060
3.199	3.227	2.285	0.2555	0.14221	23.384	18.564	1.0087
4.269	4.319	3.110	0.3445	0.19189	32.098	18.755	1.0118
6.493	6.609	4.904	0.5354	0.29880	51.569	19.164	1.0178
7.353	7.501	5.633	0.6115	0.34152	59.692	19.327	1.0201
11.527	11.872	9.284	1.0000	0.56065	102.341	20.160	1.0299
12.184	12.567	9.877	1.0632	0.59703	109.595	20.297	1.0314
19.802	20.725	17.014	1.8782	1.06250	205.023	22.042	1.0466
20.839	21.850	17.961	2.0000	1.13279	218.932	22.304	1.0485
28.517	30.216	24.928	3.0000	1.71666	332.055	24.447	1.0626
32.023	34.245	28.047	3.5234	2.02713	389.796	25.569	1.0694
34.958	37.601	30.532	4.0000	2.31278	439.512	26.591	1.0756

density between the experimental limits. The densities as a function of the linear orthogonal polynomials are as follows:

 $\begin{array}{l} - \ 0.00070 \ {\rm P^2}_{\rm C} + \ 0.00304 \ {\rm P^3}_{\rm C} \\ - \ 0.00899 \ {\rm P_T} - \ 0.00106 \ {\rm P^2}_{\rm T} \\ - \ 0.00209 \ {\rm P_C}{\rm P_T} \\ + 0.00049 \ {\rm P_C}{\rm P^2}_{\rm T} \end{array}$

Eq. 3

where

$$P_c = -1.5 -0.5 +0.5 +1.5$$

 $c' = 0 15 30 45$
 $\% (g/g)$
 $P_T = -1.5 -0.5 +0.5 +1.5$
 $T = 0 20 40 60$
(°C)

for trimethyl-1-octylammoniumbromide:

$d = 1.01996 + 0.01699 P_{c}$ 				
,	001001	Стт		Eq. 4
where $P_0 =$	-1.5	-0.5	+0.5	+1.5
c' = %(g/g)	0	16.7	33.3	50.0
$\mathbf{P}_{\mathrm{T}} =$	-1.5	-0.5	+0.5	+1.5
T = (°C)	0	20	40	60

Concentration data

Knowing the density and the molecular weights, the concentration data in different dimensions can be interconverted. Table IV and V show the interconverted data for the solutions used at 20°C. They were calculated as follows:

c' $(g_{salt}/g_{solution})$: Solutions were prepared by weighing the salt and the water. This concentration is independent of temperature.



Figure 6. Small stoppered glass tube used for equilibration of n-heptane and salt solutions.

c $(g_{salt}/cm_{solution}^3)$: c = c' · d₂₀ Eq. 5

 α (cm³_{salt}/cm³_{solution}): From the density determinations the specific volume V = 1/d can be calculated. The partial volume of the salt which satisfies (6)

$$V = \mathbf{c} \cdot \mathbf{V}_{\text{salt}} + (1 - \mathbf{c}) \cdot \mathbf{V}_{\text{H2O}}$$
Eq. 6

can easily be calculated with the aid of the equation 7

$$V_{salt} = V - c' (\partial V / \partial c')$$
Eq. 7

The volume fraction is then given by

$$\alpha = \mathbf{c} \cdot \mathbf{V}_{\text{salt}}$$
Eq. 8

x (g mole_{salt}/g mole_{solution}): For the mixture of the components a mean molecular weight can be defined which in our case is as follows:

$$\frac{1}{\mathbf{M}_{\text{solution}}} = \frac{\mathbf{c}'_{\text{salt}}}{\mathbf{M}_{\text{salt}}} + \frac{1 - \mathbf{c}'_{\text{salt}}}{\mathbf{M}_{\text{H2O}}}$$
Eq. 9

Table V. Concentrations of the aqueous solutions used of trimethyl-1-octylammoniumbromide at 20°C

\mathbf{g}/\mathbf{g}	g/cm³	cm ³ /cm ³	gmol gmol	gmol $g(H_2O)$	$\mathrm{cm^{3}}\mathrm{cm^{3}}\mathrm{(H_{2}O)}$	gmol	g/cm³
c' 100	с 100	α 100	x 100	m 1000	β 1000	Μ	d ₂₀
0.0000	0.0000	0.0000	0.0000	0.00000	0.000	18.016	0.9982
0.1034	0.1031	0.0948	0.0074	0.00410	0.949	18.033	0.9972
0.4692	0.4681	0.431	0.0337	0.01869	4.329	18.095	0.9976
1.2158	1.2139	1.116	0.0878	0.04879	11.286	18.222	0.9984
2.515	2.514	2.306	0.1839	0.10227	23.604	18.447	0.9998
3.501	3.504	3.210	0.2584	0.14383	33.165	18.621	1.0009
4.634	4.644	4.245	0.3458	0.19263	44.332	18.826	1.0021
6.801	6.831	6.223	0.5185	0.28928	66.360	19.230	1.0044
7.981	8.026	7.300	0.6156	0.34383	78.749	19.458	1.0057
12.404	12.533	11.346	1.0012	0.56136	127.981	20.361	1.0104
13.225	13.374	12.097	1.0768	0.60417	137.618	20.538	1.0113
21.493	21.927	19.734	1.9178	1.08530	245.858	22.508	1.0202
22.200	22.664	20.398	1.9972	1.13120	256.245	22.694	1.0209
30.192	31.083	27.944	2.9964	1.71455	387.809	25.035	1.0295
34.759	35.955	32.323	3.6656	2.11208	477.607	26.602	1.0344
36.799	38.146	34.331	3.9925	2.30821	522.789	27.368	1.0366

Table IVa. Concentrations of the sub	stances and markers in n-	heptane
--------------------------------------	---------------------------	---------

substance	concent	tration	marker	concentration	
	$(g/100 \text{ cm}^3_{sol})$	(gmol/l_{sol})		$(g/100_{sol})$	
ethanol	4.622	1.0	hexane	0.470	
propanol-(1)	1.207	0.2	hexane	0.492	
butanol-(1)	1.479	0.2	undecane	0.490	
pentanol-(1)	1.770	0.2	decane	0.490	
hexanol-(1)	2.040	0.2	undecane	0.488	
octanol-(1)	2.603	0.2	decane	1.452	
decanol-(1)	3.160	0.2	undecane	0.962	
dodecanol-(1)	3.720	0.2	tridecane	0.956	
dipentylether	3.171	0.2	undecane	1.439	
1-chlorooctane	2.980	0.2	undecane	1.449	
1-acetoxyoctane	3.458	0.2	dodecane	1.441	
nonanone-(2)	2.852	0.2	undecane	1.448	

where M's represent molecular weights. The mean molecular weight allows then calculation of the "g moles of the solution."

$$\eta_{\text{solution}} = \eta_{\text{salt}} + \eta_{\text{H2O}} = rac{W_{\text{solution}}}{M_{\text{solution}}}$$
Eq. 10

where w is the weight. The mean molecular weights are given in Table IV and V. Knowing the mean molecular weight, the mole fraction of the solution is given by (11)

$$\mathbf{x}_{salt} = \frac{\mathbf{c'} \cdot \mathbf{M}_{solution}}{\mathbf{M}_{salt}}$$
Eq. 11

m (g mole_{salt}/cm $^{3}_{\rm H20}$): The molality of the salt can be calculated as

$$\mathbf{m} = \mathbf{M}_{\text{salt}} \cdot \mathbf{c}' / (1 - \mathbf{c}')$$
Eq. 12

 β (cm³_{salt}/cm³_{H20}): The volume ratio is defined by (13)

$$\beta = (cV_{salt})/[(1-c) \cdot V_{H20}]$$

Eq. 13

and can easily be calculated if the function α is known and is given by

$$\beta = \alpha/(1-\alpha)$$
 Eq. 14

Determination of the partition coefficients

Equilibration of the two phases: The substance to be examined was dissolved in the organic phase (nheptane). 1 ml of this solution of known concentration was placed in a small glass tube (Figure 6), and 1 ml of the salt solution was added together with a small nickel ball. The tube was closed and fixed on an axis which was moving with a rocking motion with a period of 4 RPM under thermostatted water (20.0°C). Thus, the two phases passed over each other and in addition were mixed by the falling movement of the nickel ball.

Experiments have shown that the kinetics of the substance transport from one phase to the other had a half-life of about 20 sec. For security the two phases were equilibrated for 30 min. Finally, the tube was quickly centrifuged at room temperature, and a small part of the heptane phase was taken for gas chromatographic analysis.

Gas chromatographic analysis: All the substances investigated were chosen to be volatile for rapid concentration determination by gas chromatography. In the hydrotropic solutions used, the n-paraffins were practically insoluble. Experiments with n-decane have shown that the partition coefficient of this substance is certainly higher than 1000. Thus, these substances can be used as markers, assuming their concentrations are unchanged during the equilibration experiment. Table IVa shows the concentration of substances in n-heptane as well as those of the markers.

The concentration of the substance was taken as low as possible with the exception of the ethanol. In the latter case the partition coefficients were very low, and an analysis was only possible at higher concentrations. Proof will be given that the concentration chosen can be regarded as ideal diluted.

For the evaluation of the chromatograms a correction factor f(15) has been determined with the aid of the prepared solutions, which allows the calculation of the concentration of the substances from the ratio of the peak-areas (substance/marker). This is given from the chromatograms of the prepared solutions:

$$\mathbf{f} = \frac{\mathbf{A}_{\mathrm{s}}}{\mathbf{A}_{\mathrm{M}}} \cdot \frac{\mathbf{c}_{\mathrm{M}}}{\mathbf{c}_{\mathrm{M}}}$$
Eq. 15

where A is the peak-area in the chromatogram and c the concentration in g/cm^3 .

After equilibration, the n-heptane phases were again chromatographed and the area-ratio determined giving

$$\mathbf{c^*}_{\mathrm{S},\alpha} = (\mathbf{A'}_{\mathrm{S}}/\mathbf{A'}_{\mathrm{M}}) \cdot \mathbf{c}_{\mathrm{M}} \cdot 1/\mathrm{f}$$

Eq. 16

the index α referring to the heptane phase.

The concentration $c_{s,\alpha}$ would be the correct concentration for infinitely diluted solutions. For more concentrated solutions the substance transport during equilibration is accompanied by a volume change, δV ; i.e., the volume of the both phases after equilibration is $V\alpha_{,o} + \delta V$ and $V\beta_{,o} - \delta V$. Supposing that the substance dissolves in both phases without volume contraction, then δV is given by

$$\delta \mathbf{V} = \frac{\mathbf{V}\alpha_{,o}}{\mathbf{d}_{s}} \cdot (\mathbf{c}_{s,\alpha,o} - \mathbf{c}^{*}_{s,\alpha})$$
Eq. 17

where $V\alpha_{,0}$ is the volume of the heptane phase before equilibration. The corrected concentration is then given by (18)

$$\mathbf{c}_{\mathbf{s},\alpha} = \mathbf{c}^*_{\mathbf{s},\alpha} \cdot \frac{1}{1 - (\delta \mathbf{V} / \mathbf{V}_{\alpha,o})}$$
Eq. 18

The concentration in the salt solution (phase β) was in most cases not determined. It can be calculated if $c^*{}_{s,\alpha}$ is known:

$$c_{s,\beta} = c^* S_{,\alpha,o} - c^* s_{,\alpha} \cdot \frac{1}{1/\phi + (\delta V/V\alpha_{,o})}$$
Eq. 19

where ϕ is the phase ratio $(V\alpha_{,o}/V\beta_{,o})$

Calculation of the partition coefficients: from the above results the partition coefficients can be calculated as:

$$\mathrm{K_{c}}=\mathrm{c_{s,lpha}/c_{s,eta}}$$
 Eq. 20

Tables V and VI show the experimentally determined partition coefficients, K_c , and their logarithms as well as two other partition coefficients (K_m and K_x , see below) with their logarithms, which can be calculated from K_c :

a) if the concentration of the substance is given in mass of substance per mass of solution, the partition coefficient K_m can be calculated:

$$K_{\rm in} = K_{\rm e} \cdot (d\beta/d\alpha) = K_{\rm e} \cdot \frac{d_{\rm solution}}{d_{\rm heptane}}$$

$$F_{\rm e} \cdot \frac{d_{\rm solution}}{d_{\rm heptane}}$$

for the ideal diluted case.

b) if the concentration of the substance is given in mole fraction or mole % the partition coefficient changes into:

$$\mathbf{K}_{x} \!=\! \mathbf{K}_{e} \! \cdot \! \frac{\mathbf{d}_{\text{solution}}}{\mathbf{d}_{\text{heptane}}} \; \frac{\mathbf{M}_{\text{heptane}}}{\mathbf{M}_{\text{solution}}} \\ \mathbf{Eq. 22}$$

Dependence of the partition coefficients on the substance concentration: Tables VII and VIII show the logarithms of the partition coefficients K_c at different salt concentrations and with different sub-

			Ethanol		Propanol-(1)		Butanol-(1)		Pentanol- (1)		Hexan	ol-(1)
c'	-log γ		K	log k	к	log K	K	log K	K	log K	K	log K
0.0000	0.00000	K _c K _m	0.00773 0.0113 0.0628	0.888 -3 0.053 -2 0.798 -2	0.0246 0.0345 0.200	0.391 -2 0.555 -2 0 301 -1	0.127 0.185 1.032	0.104 -1 0.268 -1 0.014	1.242 1.814 10.09	0.094 0.259 1.004	6.12 8.94 49.7	0.787 0.951 1.696
0.0953	0.03009	$f K_{ m c} \ K_{ m m} \ K_{ m x}$	0.0028 0.00437 0.00639 0.0355	0.640 -3 0.805 -3 0.550 -2	0.0232 0.0339 0.189	0.366 -2 0.530 -2 0.276 -1	0.141 0.206 1.145	0.149 -1 0.314 -1 0.059	1.288 1.881 10.46	0.110 0.275 1.020	6.77 9.90 55.5	0.831 0.996 1.744
0.4322	0.06011	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$	0.00668 0.00978 0.0542	0.825 -3 0.990 -3 0.734 -2	0.0241 0.0353 0.195	0.382 -2 0.548 -2 0.290 -1	0.129 0.189 1.045	0.111 -1 0.276 -1 0.019	1.134 1.659 9.19	0.055 0.220 0.963	6.57 9.61 53.2	0.818 0.983 1.726
1.1201	0.09042	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$	0.00437 0.00641 0.0353	0.640 -3 0.807 -3 0.548 -2	0.0241 0.0353 0.1945	0.382 -2 0.548 -2 0.289 -1	0.135 0.198 1.089	0.131 -1 0.297 -1 0.037	1.212 1.776 9.78	0.084 0.250 0.990	5.37 7.87 43.4	0.730 0.896 1.638
2.317	0.12106	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathbf{x}} \end{array}$	0.00367 0.00540 0.0294	0.565 -3 0.732 -3 0.469 -2	0.0250 0.0368 0.200	0.398 -2 0.566 -2 0.301 -1	0.136 0.200 1.088	0.134 -1 0.301 -1 0.037	1.161 1.709 9.29	0.065 0.233 0.968	6.54 9.62 52.3	0.816 0.984 1.719
3.199	0.13692	K _c K _m K _x										
4.269	0.15231	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$	0.00322 0.00477 0.0255	0.508 -3 0.679 -3 0.406 -2	0.0232 0.0343 0.1834	0.366 -2 0.535 -2 0.263 -1	0.116 0.172 0.917	0.065 -1 0.235 -1 0.962 -1	0.555 0.822 4.39	0.744 -1 0.915 -1 0.642	1.968 2.91 15.55	0.294 0.464 1.192
6.493	0.17672	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$										
7.353	0.18443	K _c K _m K _x	0.00390 0.00582 0.0302	0.591 -3 0.765 -3 0.480 -2	0.0223 0.0333 0.1725	0.349 -2 0.522 -2 0.237 -1	0.0889 0.1326 0.688	0.949 -2 0.123 -1 0.838 -1	0.272 0.406 2.10	0.435 -1 0.609 -1 0.323	0.574 0.856 4.44	0.759 -1 0.932 -1 0.647
11.527	0.21409	$f K_{ m c} \ K_{ m m} \ K_{ m x}$										
12.184	0.21794	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathbf{x}} \end{array}$	0.00390 0.00588 0.0290	0.591 -3 0.769 -3 0.463 -2	0.0215 0.0324 0.1600	0.332 -2 0.511 -2 0.204 -1	0.0635 0.0957 0.473	0.803 -2 0.981 -2 0.675 -1	0.1489 0.225 1.107	0.173 -1 0.352 -1 0.044	0.275 0.415 2.05	0.439 -1 0.618 -1 0.311
19.802	0.25379	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathtt{x}} \end{array}$	0.00483 0.00739 0.0336	0.684 -3 0.869 -3 0.526 -2	0.0180 0.0276 0.1251	0.225 -2 0.441 -2 0.098 -1	0.0460 0.0704 0.320	0.663 -2 0.848 -2 0.505 -1	0.0950 0.1454 0.661	0.978 -2 0.162 -1 0.820 -1	0.140 0.214 0.974	0.147 -1 0.331 -1 0.988 -1
20.839	0.25779	$f K_e \ K_m \ K_x$										
28.517	0.28357	$f K_{ m c} K_{ m m} K_{ m m} K_{ m x}$										
32.023	0.29371	$f K_c \ K_m \ K_x$	0.00503 0.00787 0.0308	0.702 -3 0.896 -3 0.489 -2	0.0154 0.0241 0.0944	0.187 -2 0.382 -2 0.975 -2	0.0349 0.0546 0.214	0.542 -2 0.732 -2 0.330 -1	0.0560 0.0876 0.343	0.748 -2 0.943 -2 0.535 -1	0.0724 0.1132 0.444	0.860 -2 0.054 -1 0.647 -1
34.958	0.30166	K _c K _m K										

Table V. Partition coefficients between heptane and aqueous solutions of potassium-1-octylsulfonate

Table V. (Continued)Partition coefficients between heptane and aqueoussolutions of potassium-1-octylsulfonate

			$Octanol_{-}(1)$		Decanol-(1)		Dodecanol(1)		1-Chloro- octane		Octanol-(1) -acetate		Nona- none (2)	
C'	-log γ		K	log K	K	log K	K	log K	K	log K	K	log K	K	log K
0.0000	0.00000	K _c K _m K _x	147 215 1194	2.167 2.332 3.077	7880 11500 64000	3.896 4.061 4.806								
0.0953	0.03009	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$												
0.4322	0.06011	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$												
1.1201	0.09042	K _e K _m K _x	(250) (366) (2020)	(2.398) (2.564) (3.305)										
2.317	0.12106	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$												
3.199	0.13692	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$	21.9 32.3 174	1.340 1.509 2.241										
4.269	0.15231	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathbf{x}} \end{array}$	7.45 11.02 58.90	0.872 1.042 1.770	23.3 34.5 184	1.368 1.538 2.265	28.0 41.5 221.0	1.447 1.618 2.344						
6.493	0.17672	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathbf{x}} \end{array}$	1.94 2.89 15.1	0.287 0.461 1.179										
7.353	0.18443	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$			2.91 4.34 22.5	0.464 0.638 1.352	4.20 6.27 32.5	0.624 0.797 1.512	57.5 85.8 445	1.759 1.934 2.648			65 97 503	1.815 1.987 2.701
11.527	0.21409	K _c K _m K _x	0.620 0.934 4.64	0.792 -1 0.970 -1 0.667										
12.184	0.21794	$egin{array}{c} \mathbf{K}_{\mathbf{c}} \ \mathbf{K}_{\mathbf{m}} \ \mathbf{K}_{\mathbf{x}} \end{array}$			0.909 1.37 6.77	9 0.958 -1 1 0.137 0.831	1.35 2.04 10.05	0.130 0.310 1.002	34.5 52.0 257	1.538 1.716 2.410	34.3 51.7 255	1.536 1.714 2.407	24.0 36.2 179	1.381 1.559 2.252
19.802	0.25379	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$			0.381 0.583 2.65	0.581 -1 0.766 -1 0.423	0.507 0.776 3.53	0.705 -1 0.890 -1 0.547	19.6 30.0 136	1.292 1.477 2.134	20.4 31.2 142	1.310 1.494 2.152	9.92 15.2 69.0	0.997 1.181 1.839
20.839	0.25779	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathtt{x}} \end{array}$	0.219 0.336 1.508	0.340 -1 0.526 -1 0.179										
28.517	0.28357	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$	0.151 0.235 0.962	0.179-1 0.371 -1 0.983 -1										
32.023	0.29371	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$			0.170 0.266 1.04) 0.231 -1 5 0.425 -1 1 0.018	0.206 0.322 1.262	0.314 -1 0.508 -1 0.101	13.5 21.1 82.8	1.130 1.324 1.918	6.04 9.44 37.0	0.781 0.975 1.568	3.83 6.00 23.5	0.583 0.778 1.371
34.958	0.30166	$f K_c K_m K_m K_x$	0.111 0.175 0.658	0.047 -1 0.243 -1 0.818 -1										

Table VI. Partition coefficients between heptane and aqueous solutions of trimethyl-1-octylammoniumbromide

			Et	hanol	Prop	anol-(1)	Buta	nol-(1)	Penta	nol-(1)	Hexan	ol-(1)
C′	-log γ		ĸ	log K	ĸ	log K	K	log K	ĸ	log K	K	log K
0.0000	0.00000	K _c K _m K _x	0.00773 0.0113 0.0628	0.888 -3 0.053 -2 0.798 -2	0.0246 0.0345 0.200	0.391 -2 0.538 -2 0.301 -1	0.127 0.185 1.032	0.104 -1 0.268 -1 0.014	1.242 1.814 10.09	0.094 0.259 1.004	6.12 8.94 49.7	0.787 0.951 1.696
0.1034	0.03009	K _c K _m K _x	0.00575 0.00839 0.04659	0.760 -3 0.924 -3 0.669 -2	0.0241 0.0351 0.1953	0.383 -2 0.545 -2 0.291 -1	0.129 0.188 1.045	0.111 -1 0.274 -1 0.019	1.150 1.677 9.319	0.061 0.225 0.969	5.91 8.62 47.89	0.772 0.936 1.680
0.4692	0.06014	$f K_{m} \ K_{m} \ K_{x}$	0.00413 0.00603 0.03337	0.616 -3 0.780 -3 0.523 -2	0.0259 0.0378 0.2092	0.413 -2 0.577 -2 0.321 -1	0.123 0.179 0.994	0.090 -1 0.254 -1 0.997 -1	1.246 1.818 10.067	0.096 0.260 1.003	6.13 8.94 49.52	0.787 0.951 1.695
1.2158	0.09047	K _c K _m K _x	0.00391 0.00571 0.03139	0.592 -3 0.757 -3 0.497 -2	0.0259 0.9378 0.2080	0.413 -2 0.577 -2 0.318 -1	0.129 0.188 1.036	0.111 -1 0.274 -1 0.015	1.246 1.819 10.00	0.096 0.260 1.000	7.48 10.92 60.06	0.874 1.038 1.779
2.515	0.12116	$f K_{ m c} \ K_{ m m} \ K_{ m x}$	0.00391 0.00572 0.03105	0.592 -3 0.757 -3 0.492 -2	0.0250 0.0366 0.1986	0.398 -2 0.563 -2 0.298 -1	0.123 0.180 0.977	0.090 -1 0.255 -1 0.990 -1	1.101 1.610 8.744	0.042 0.027 0.942	7.21 10.54 57.26	0.858 1.023 1.758
3.501	0.13749	K _e K _m K _x										
4.634	0.15251	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$	$\begin{array}{c} 0.00413 \\ 0.00605 \\ 0.03222 \end{array}$	0.616 -3 0.782 -3 0.508 -2	0.0241 0.0353 0.1880	0.382 -2 0.548 -2 0.274 -1	0.159 0.233 1.240	0.201 -1 0.367 -1 0.093	1.074 1.574 8.378	0.031 0.197 0.923	6.95 10.19 54.21	0.842 1.008 1.734
6.801	0.17487	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$										
7.981	0.18482	K K K	0.00391 0.00575 0.02961	0.592 -3 0.760 -3 0.471 -2	0.0241 0.0354 0.1825	0.382 -2 0.549 -2 0.261 -1	0.1045 0.1537 0.7915	0.019 -1 0.187 -1 0.898 -1	0.572 0.841 4.332	0.757 -1 0.925 -1 0.637	1.83 2.69 13.86	0.262 0.430 1.142
12.404	0.21416	K _c K _m K _x										
13.225	0.21868	K _c K _m K _x	0.00391 0.00578 0.02821	0.592 -3 0.762 -3 0.450 -2	0.0215 0.0318 0.1551	0.332 -2 0.502 -2 0.190 -1	0.0782 0.1156 0.5643	0.893 -2 0.063 -1 0.751 -1	0.250 0.370 1.804	0.398 -1 0.568 -1 0.256	0.502 0.742 3.622	0.701 -1 0.870 -1 0.559
21.493	0.25512	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$	0.00460 0.00686 0.03055	0.663 -2 0.836 -3 0.485 -2	0.0189 0.0282 0.1255	0.276 -2 0.450 -2 0.098 -1	0.0574 0.0856 0.3812	0.759 -2 0.932 -2 0.581 -1	0.138 0.206 0.916	0.140 -1 0.314 -1 0.962 -1	0.213 0.318 1.415	0.328 -1 0.502 -1 0.151
22.200	0.25771	K _e K _m K _x										
30.192	0.28350	K _c K _m K _x										
34.759	0.29620	$f K_c \ K_m \ K_x$	0.00483 0.00731 0.02752	0.684 -3 0.864 -3 0.440 -2	0.0171 0.0259 0.0974	0.233 -2 0.413 -2 0.989 -2	0.0475 0.0719 0.2707	0.677 -2 0.857 -2 0.432 -1	0.0834 0.1262 0.4752	0.921 -2 0.101 -1 0.677 -1	0.115 0.174 0.655	0.059 -1 0.241 -1 0.816 -1
36.799	0.30153	K _c K _m K _x										

		Octanol-(1)		Decanol(1)		Dodecanol-(1)		Nonanone (2)		n-Diamylether		
C'	-log γ		K	log K	К	log K	K	log K	K	log K	K	log K
0.0000	0.00000	K _c K _m K _x	147 215 1194	1.167 2.332 3.077	7880 11500 64000	3.896 4.061 4.806						
0.1034	0.03009	K _c K _m K _x										
0.4692	0.06014	$f K_c K_m K_m K_x$										
1.2158	0.09047	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathrm{x}} \end{array}$										
2.515	0.12116	·K _e K _m K _x	(172) (251) (1366)	(2.235) (2.400) (3.136)								
3.501	0.13749	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathbf{x}} \end{array}$	56.4 82.6 444.2	1.751 1.917 2.647								
4.634	0.15251	$f K_e \ K_m \ K_x$	(212) (311) (1654)	(2.326) (2.493) (3.219)								
6.801	0.17487	$egin{array}{c} \mathbf{K}_{\mathrm{c}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathbf{x}} \end{array}$	31.2 45.8 238.8	1.494 1.661 2.377								
7.981	0.18482	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathbf{x}} \end{array}$	11.6 17.1 87.9	1.065 1.233 1.944					46.6 68.5 352.9	1.668 1.836 2.548	36.8 54.1 278.7	1.566 1.733 2.445
12.404	0.21416	$f K_c \ K_m \ K_x$	1.65 2.44 12.00	0.218 0.387 1.079								
13.225	0.21868	K _c K _m K _x			$3.50 \\ 5.18 \\ 25.25$	0.544 0.714 1.402	8.07 11.93 58.23	0.907 1.077 1.765	23.2 34.3 167.4	1.365 1.535 2.223	34.8 50.6 246.8	$1.534 \\ 1.704 \\ 2.392$
21.493	0.25512	$egin{array}{c} \mathbf{K}_{\mathrm{e}} \ \mathbf{K}_{\mathrm{m}} \ \mathbf{K}_{\mathtt{x}} \end{array}$			0.896 1.337 5.951	0.952 -1 0.126 0.775	$1.72 \\ 2.57 \\ 11.42$	0.235 0.410 1.058	11.8 17.6 78.4	1.072 1.246 1.894	29.5 44.0 195.9	$1.470 \\ 1.643 \\ 2.292$
22.200	0.25771	$f K_{ m c} \ K_{ m m} \ K_{ m x}$	0.445 0.666 2.940	0.649 -1 0.823 -1 0.468								
30.192	0.28350	K _c K _m K _x	0.251 0.378 1.513	0.399 -1 0.577 -1 0.180								
34.759	0.29620	K _c K _m K _x			0.313 0.474 1.783	0.495 -1 0.676 -1 0.251	0.536 0.811 3.054	0.729 -1 0.909 -1 0.485	5.36 8.11 30.54	0.729 0.909 1.485	30.1 45.5 171.5	1.479 1.658 2.234
36.799	0.30153	K _c K _m K _x	0.182 0.276 1.010	0.260 -1 0.441 -1 0.005								

Table VI. (Continued) Partition coefficients between heptane and aqueous solutions of trimethyl-1-octylammoniumbromide

stance concentrations in the case of octanol(1).

Variance analysis of the results have shown that within experimental error, there is no significant change in log K especially for concentrations not higher than 0.2 m. Therefore, for all other experiments, the concentration 0.2 m. was chosen as high enough for analysis but low enough to be ideally diluted (see also Table IVa).

Apparatus

Construction and function (see Figure 1 and 2): The eluent is filled into a glass container (1) of internal diameter 20 cm and capacity 5 l. This container is connected through a three-way tap (3) which can be turned in two positions, either allowing the eluent to flow into the line and the burette (2), or (position in Figure 2) connecting only the burette with the line. This second position allows the sampleloading: the burette is emptied by pumping away the eluent and then the substance, diluted with the eluent, is filled into the burette. After loading, the tap is turned to the first position (connecting burette, container, and line).

The eluent passes through a sintered metal filter (4) and to a solution metering pump (5) (Beckman Model 746, 0-20 ml/min) which determines the velocity of the eluent with a precision of about 2%. After the pump is an excess pressure valve giving a back pressure of about $\frac{1}{2}$ atm. At N a slow nitrogen stream (\sim 2-3 ml/min) is pressed into the eluent which then enters the separation tube (7). The tubes can be rotated with the aid of an electric motor (9) with a speed of up to 140 RPM. The separation tubes are connected by small bore stainless steel tubes 3 mm i.d. The whole apparatus is inclined to an extent that both the separation tubes and the connection tubes are descending for the movement of the eluent. After passing through all the tubes, the eluent is led to an overflow (10) where the main stream is collected (12). A bypass from the overflow goes to the detector (11) where the refraction index is measured continuously (Waters liquid chromatography, Model R 4) and is registered on a recorder.

For the description of the separation tubes see Figure 1 and the explanation in part one.

Table VII. Logarithms of the partition coefficients K_c of octanol-(1) between n-heptane and aqueous solutions of potassium-1-octylsulfonate

initial conc octanol	entration l-(1)	co	oncentrat	ion of the	e salt (g/i	100 g _{soluti}	_{on})
$(g/100 \text{ cm}^3)$	(mole/l)	3.2	6.5	11.5	20.8	28.5	35.0
1.3	0.1	1.286	0.202	0.298	0.700	0.816	0.970
2.6	0.2	1.482	0.370	0.220	0.688	0.842	0.940
3.9	0.3	1.625	0.403	0.151	0.638	0.822	0.952
5.2	0.4	1.477	0.460	0.064	0.594	0.794	0.948

Table VIII. Logarithms of the partition coefficients K_c of octanol-(1) between n-heptane and aqueous solutions of trimethyl-1-octylammoniumbromide.

initial concentration

octanol	-(1)	co	concentration of the salt $(g/100 g_{solution})$							
$(g/100 \text{ cm}^3)$	(mole/l)	3.5	6.8	12.4	22.2	30.2	36.8			
1.3	0.1	1.514	1.471	0.176	0.373	0.579	-0.725			
2.6	0.2	1.891	1.718	0.218	0.367	0.615	0.741			
3.9	0.3	1.943	1.483	0.257	0.328	0.611	0.744			
5.2	0.4	1.819	1.463	0.285	0.320	0.591	0.748			

The apparatus can, of course, also be used with a smaller number of separation tubes.

Filling the separation tubes with the two phases: The tube is first placed in a horizontal position and filled completely with a solution of the hydrotropically active salt (or other solvent). By inclining the tube to a given angle, which of course must be higher than the position of the tube in the apparatus, a fraction of the stationary phase flows out. The tube is now placed into the apparatus and filled with the mobile phase without rotating in order to avoid foaming of the solution. After all the tubes are filled with the eluent, they can be rotated and the separation can be started.

Acknowledgment

This work was financially supported by Firmenich & Cie., Geneva, Switzerland. We gratefully acknowledge the help in the experimental part of Heinz Fischer, Roland Ott, and Alderich Tresch.

Literature Cited

- 1. Rath, H., Rau, J., and Wagner, D., Melliand Textilber. 43, 718 (1962).
- 2. Michaelis, W., Schindler, O., and Signer, R., Helv. Chim. Acta **48**, 42 (1965).
- 3. Arn, H., Grob, E. C., and Signer, R., Helv. Chim. Acta 48, 851 (1965).
- Signer, R., Allemann, K., Koehli, E., Lehmann, W., Meyer, H., and Ritschard, W., Dechema Monograph. 27, 32 (1956).
- 5. Signer, R., and Arn, H., Helv. Chim. Acta (in press).
- Neuberg, C., Biochem. Z. 76, 107 (1916).
- Rath, H., Rau, J., and Wagner, D., Melliand Textilber. 44, 969 (1963).
- Kovats, E. sz., Z. Anal. Chem. 181, 351 (1961). See also Kovats, E. sz., Advances of Chromatography, Vol. 1, J. C. Giddings and R. A. Keller, editors, M. Dekker, Inc., New York, 1965, p. 229.
- Kovats, E. sz., and Weiss, P. B., Ber. Bunsenges. Physik. Chem. 69, 812 (1965).
- Backer, H. J., Rec. Trav. Chim. 48, 949 (1929).

Manuscript received January 25, 1967